





19 AIChE
Spring Meeting

15TH
GLOBAL
CONGRESS
ON **PROCESS**
SAFETY



NEW ORLEANS • 2019

March 31 – April 4, 2019
Hilton New Orleans Riverside



Unique Applications for Embedded Model Predictive Control Technology

Paper 137a

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April 2, 2019

Speaker – James Beall

- Principal Process Control Consultant with Emerson Automation Solutions since 2001
- 37+ Years experience with Petrochemical Process Automation
- Specialist in advanced regulatory control and multivariable control
- Eastman Chemical Company, Texas Operations (1981-2001)

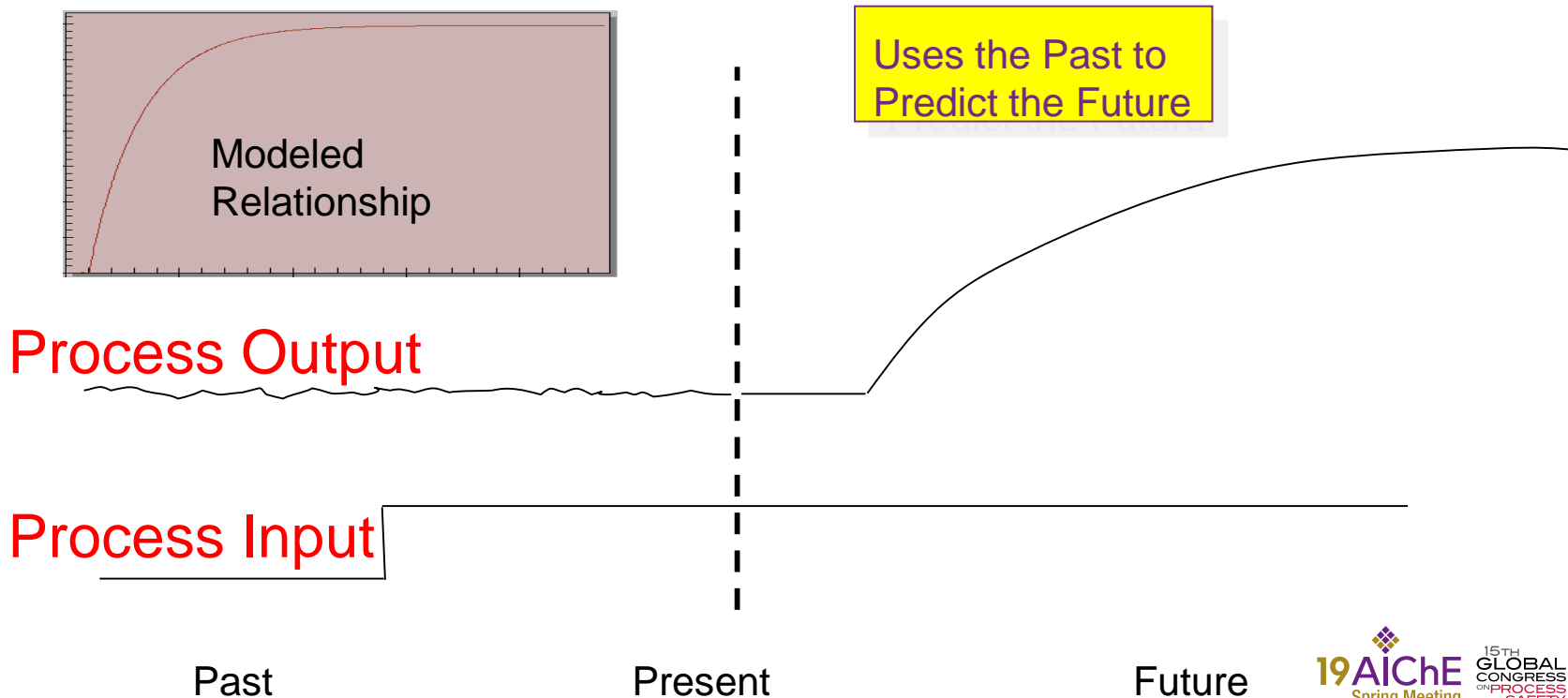




Introduction

- What is MPC?
- What is Embedded MPC?
- Example Uses of Embedded MPC
- Questions

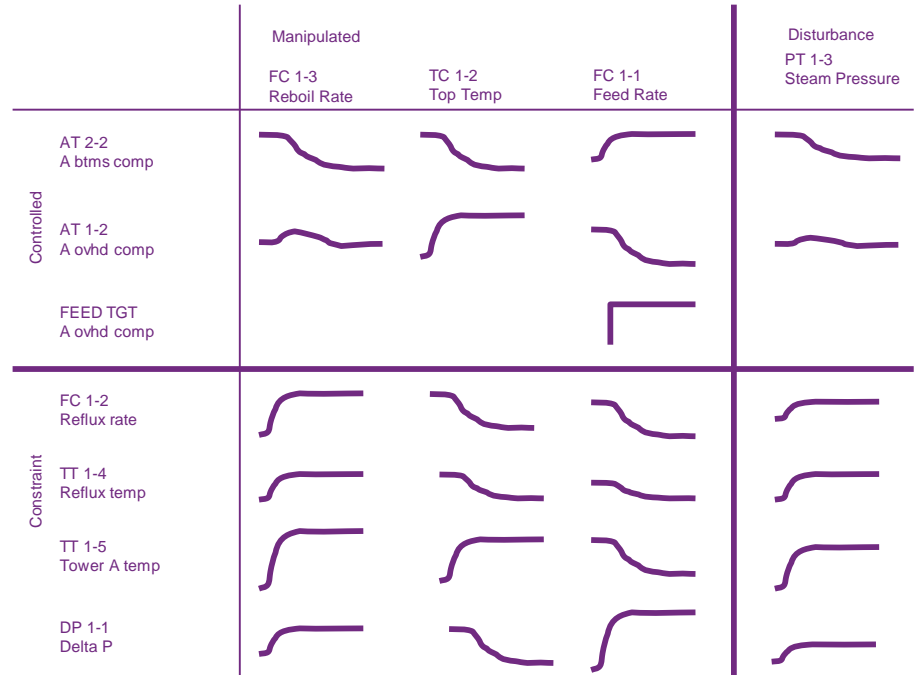
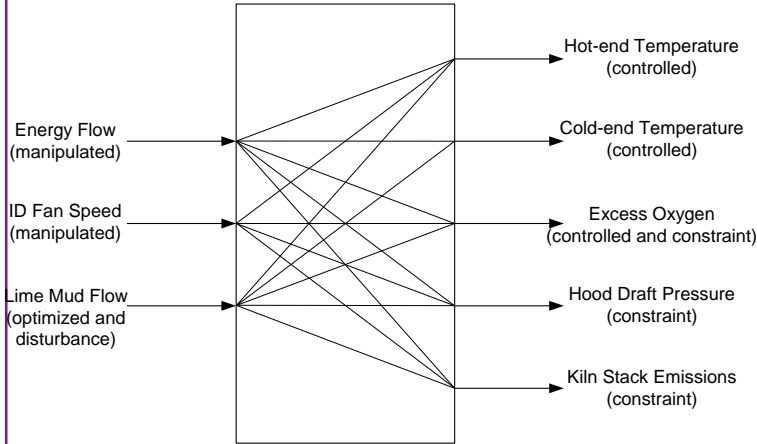
“MPC”: Multivariable, *Model* Predictive Controller





“MPC”: *Multivariable*, Model Predictive Controller

Lime Kiln Process

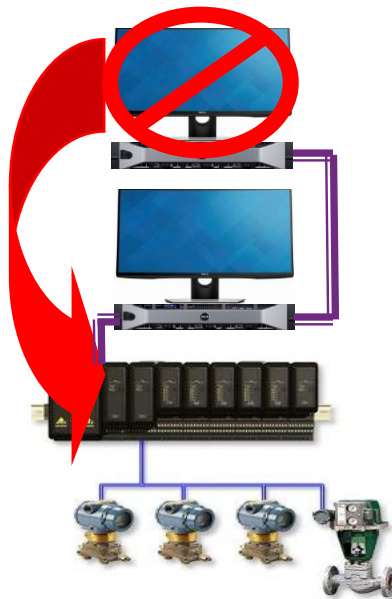


What is *Embedded MPC*?

Embedded MPC:

- NO extra databases
- NO database synchronization issues
- NO watchdog timers
- NO fail/shed logic design
- NO custom DCS programming
- NO interface programming
- NO operator interface development

Traditional APC

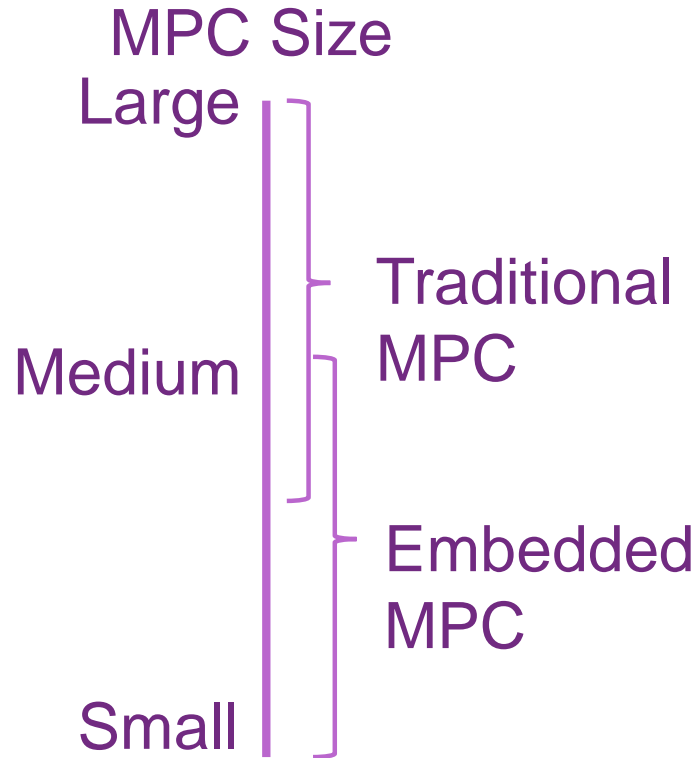


Embedded MPC:

- Can run in DCS controllers/stations
- Redundant and fast (e.g. 1/sec)
- Integrated operator user interface
- Configuration through standard configuration tools
- Automated step testing and Model ID
- Off-line simulation and testing
- Implementation by plant control engineers



Traditional and Embedded MPC



- Traditional MPC

- Well developed, full featured technology
- Higher “minimum” project cost
- Medium to larger req’d for ROI

- Embedded MPC

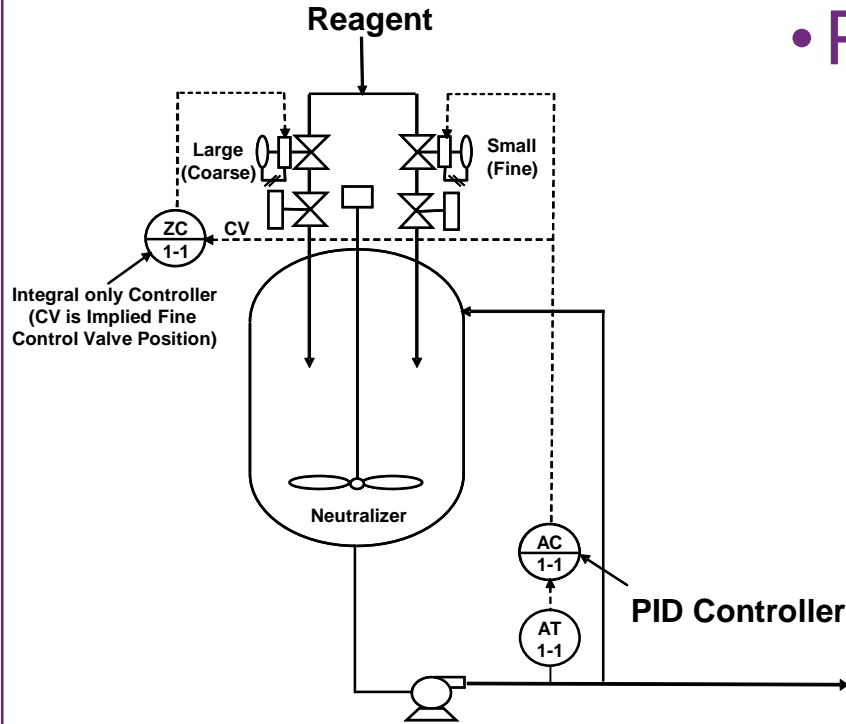
- Less features to “fit” in DCS
- Lower implementation cost
- ROI for smaller



Examples of Unique Applications

- “Big Valve, Little Valve”
- Dead time dominant SISO
- Feed Forward and Override
- Waste heat steam generator
- Waste heat recovery – steam export

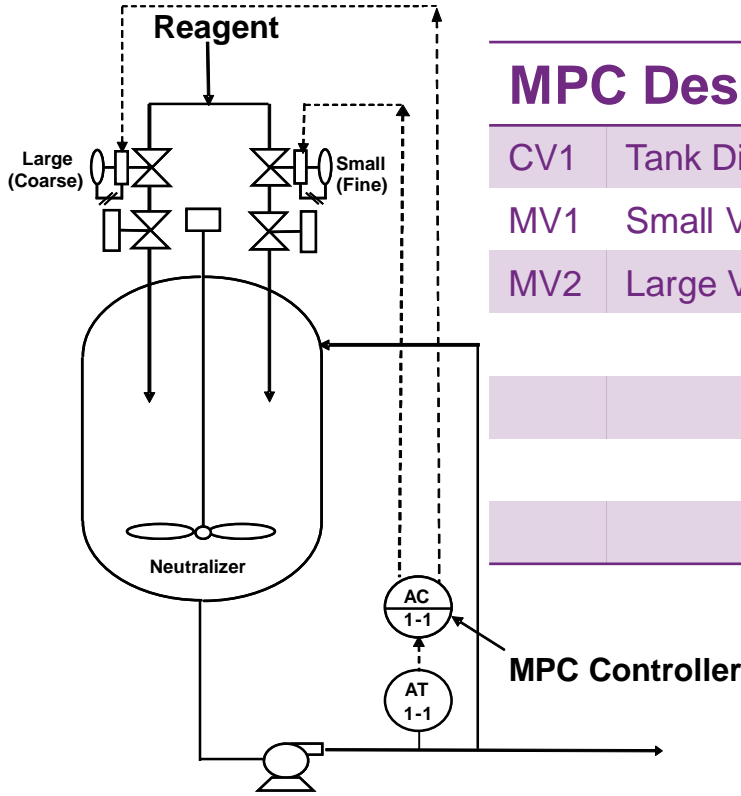
“Big Valve, Little Valve”



• PID Considerations

- Large PV disturbances can saturate Small valve – loss of control
- ZC should have “gap” control to eliminate potential Large valve limit cycles

“Big Valve, Little Valve”



MPC Design

CV1	Tank Discharge pH
MV1	Small Valve
MV2	Large Valve

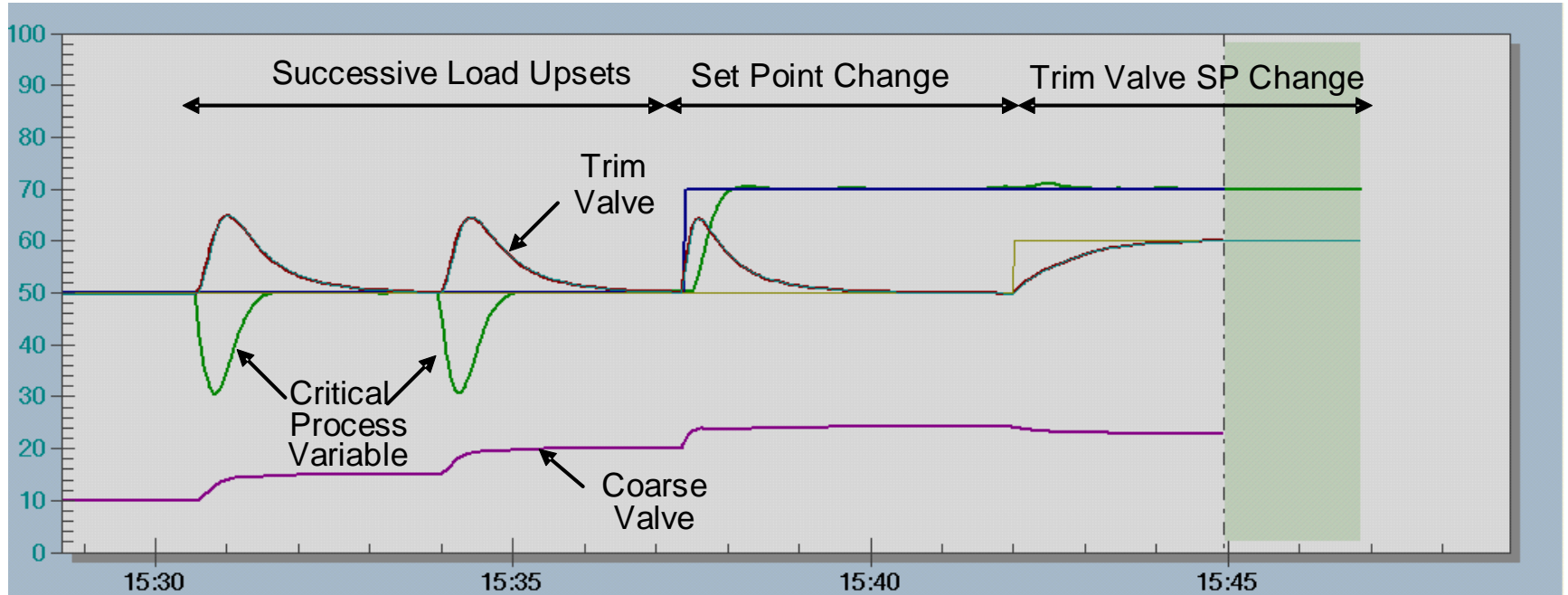
MPC Considerations

- Large PV disturbances handled by moving both Large and Small valves
- Use constraint control on small valve position to eliminate large valve limit cycles



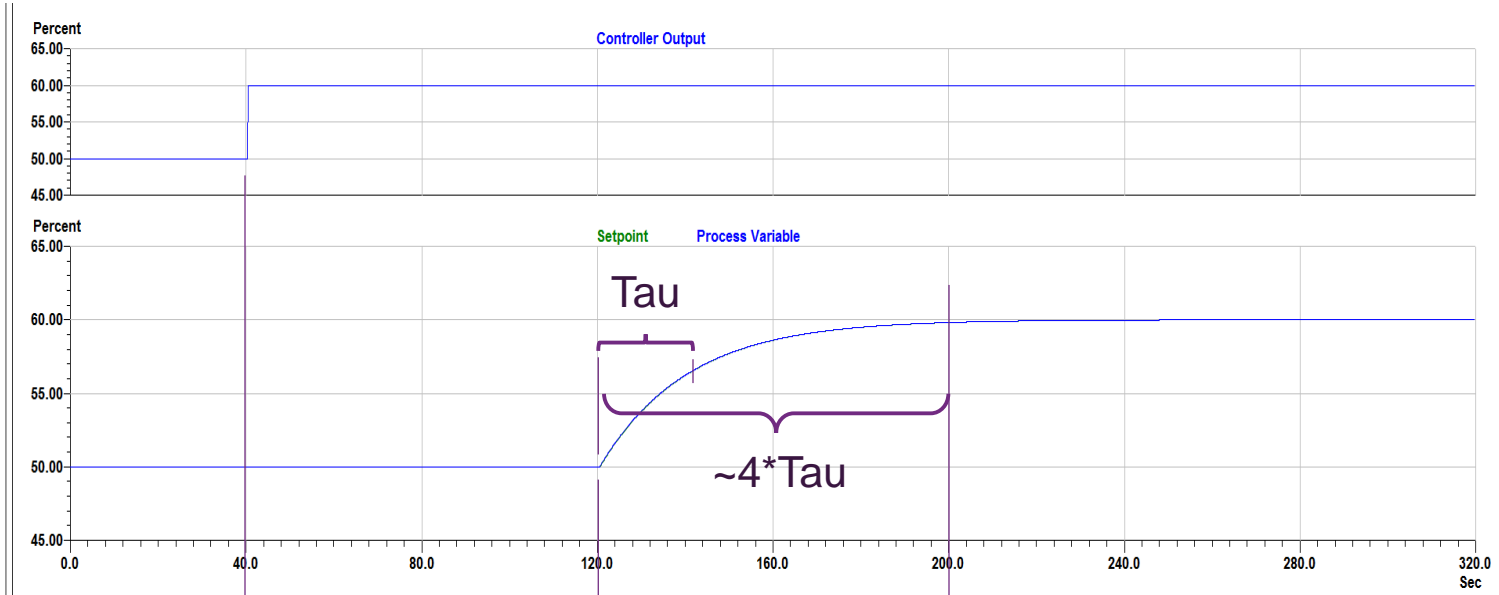
“Big Valve, Little Valve”

MPC Performance



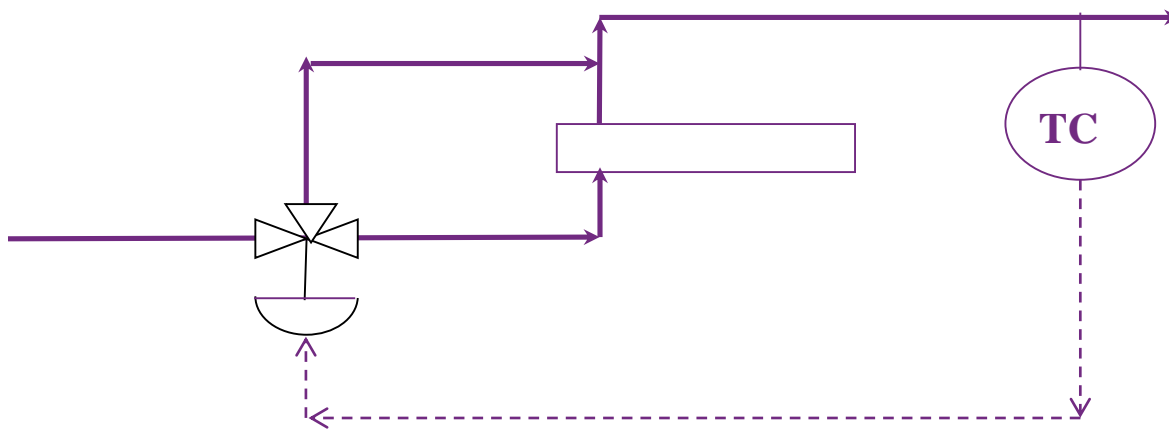


Deadtime Dominant Loops



↑ ↑
Dead time $\geq 4 \cdot \tau$ (definition varies)

Deadtime Dominant Loop

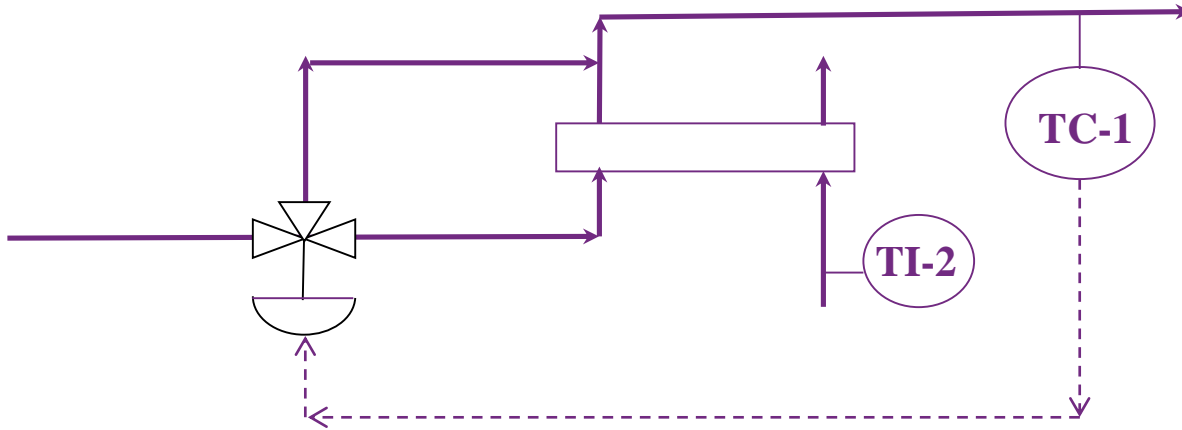


MPC Variables

CV1	Coolant Temperature
MV1	3-Way Valve

- Reactor coolant supply temperature
- “Mixing” temperature response fast (~ 15 sec τ)
- Step test revealed 80 seconds of dead time!

Feed Forward with MPC

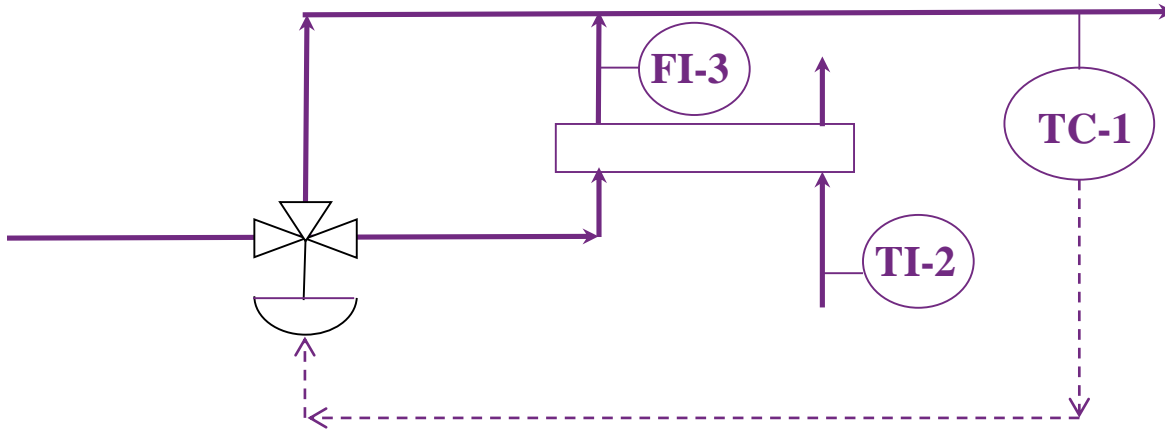


MPC Variables

CV1	Coolant Temperature
MV1	3-Way Valve
DV1	Cooling Water Temp

- Temperature of cooling water impacts outlet temp
- Typically implemented as feedforward to PID (calculate FFWD Gain, dead time, lead-lag)
- Use TI-2 as a Disturbance Variable with MPC-simple model

Override/Constraint with MPC



MPC Variables

CV1	Coolant Temperature
CV2	Minimum Tube Flow
MV1	3-Way Valve
DV1	Cooling Water Temp

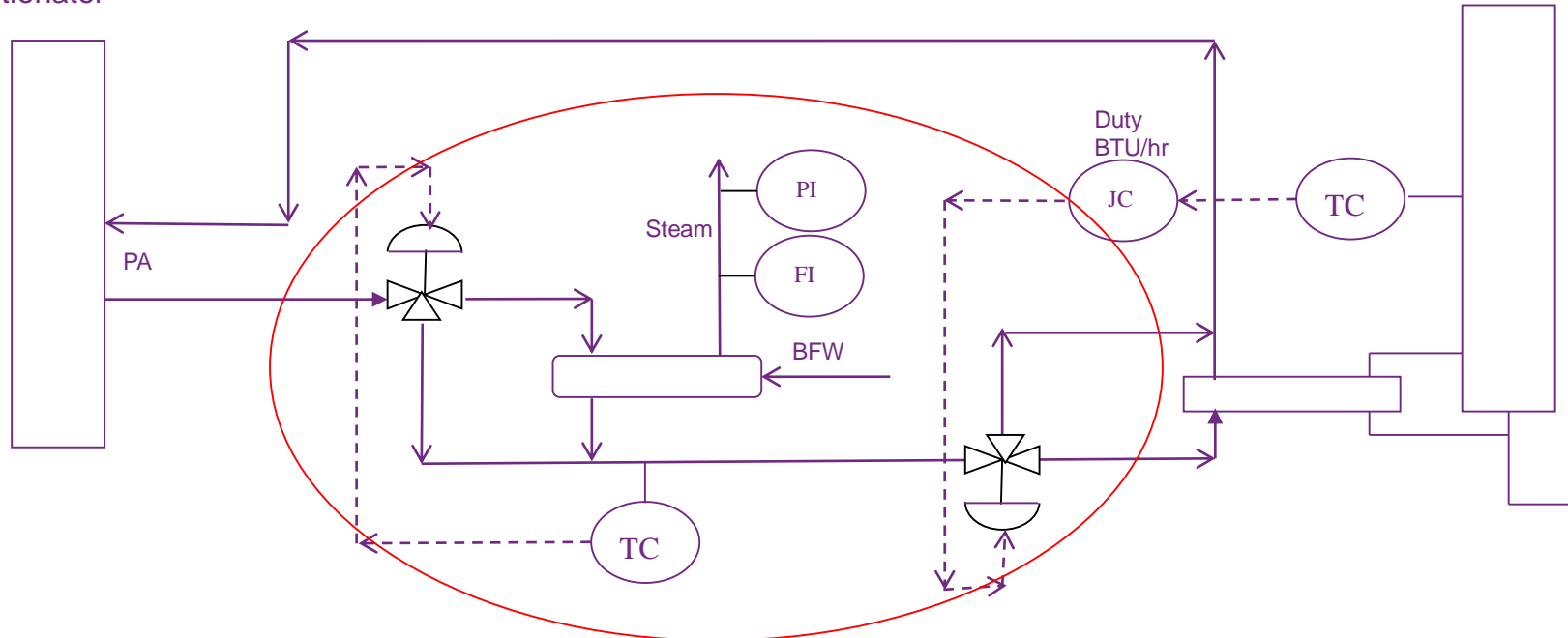
- Suppose there is a minimum flow through exchanger tubes, FI-3, to avoid fouling
- Typically done with 2 PID's and a hi/lo selector
- Implement as a Constraint Variable (LV) with MPC



Optimize Small Applications

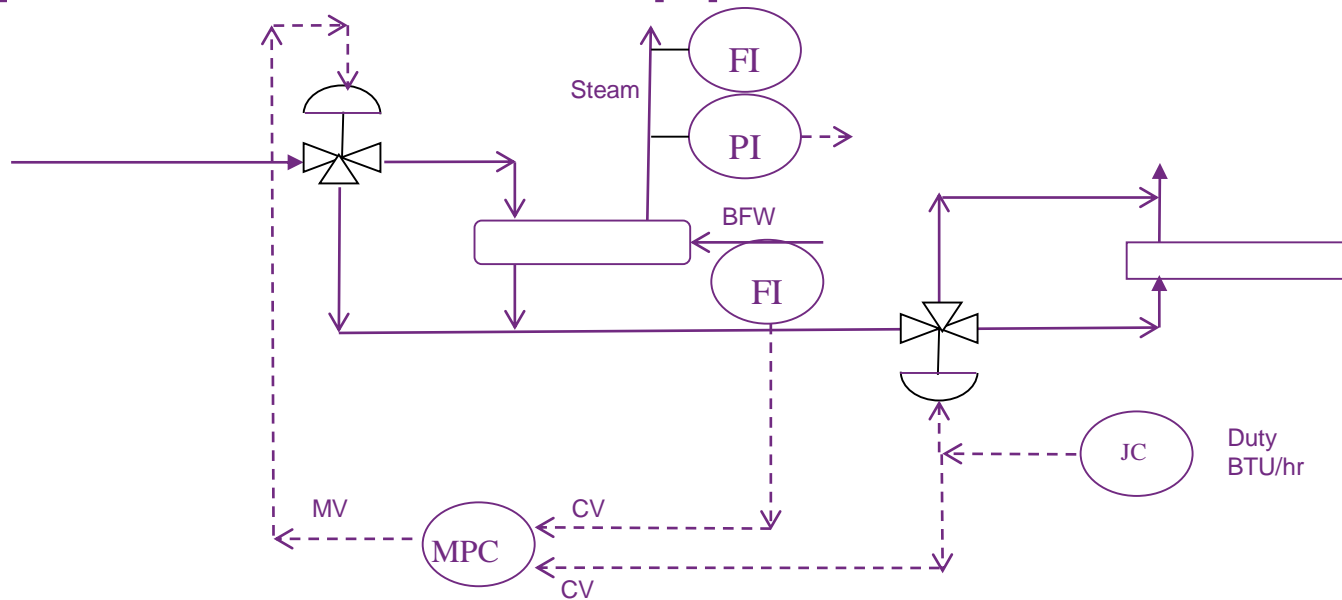
Fractionator

Debutanizer



Goal is to maximize steam production while ensuring sufficient heat for debutanizer reboiler. Also, handle limited BFW supply.

Optimize Small Applications



Objective: Maximize steam production

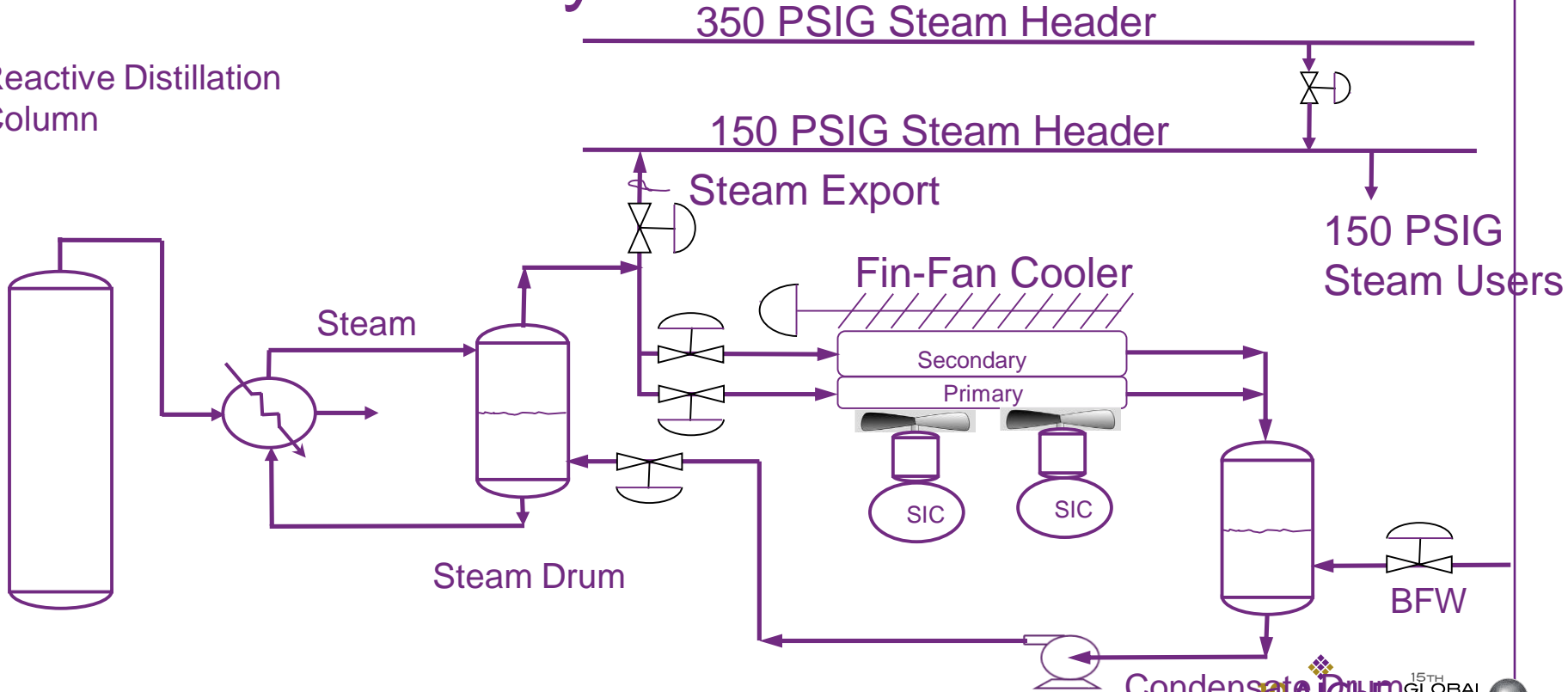
Implementation time: 2 days

Benefit: \$120K/year



Heat Recovery

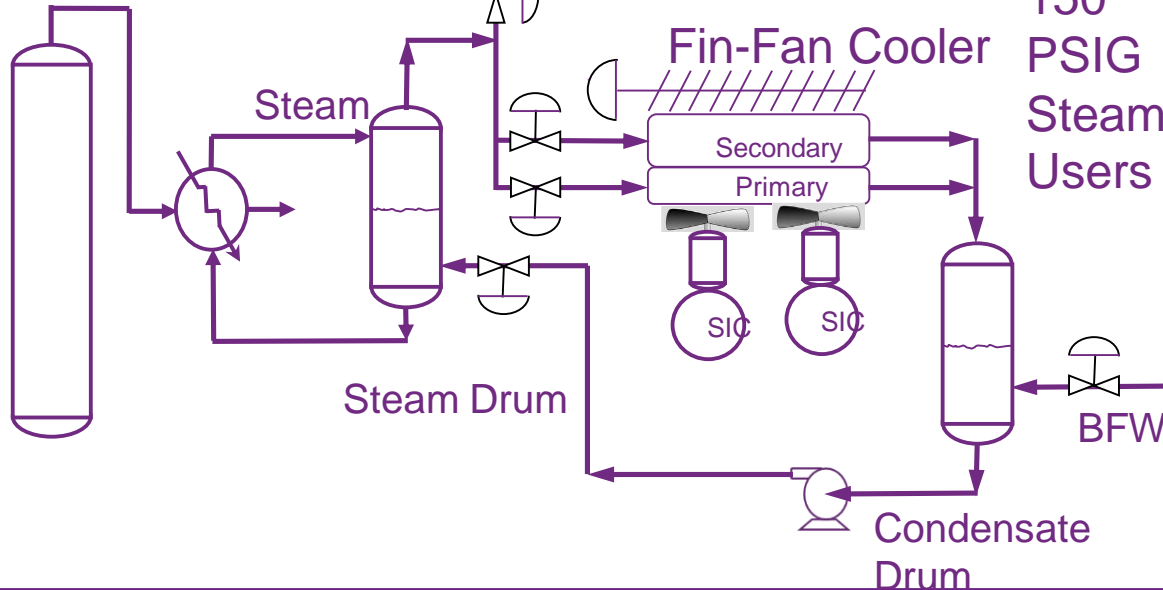
Reactive Distillation Column





Heat Recovery

Reactive
Distillation
Column



MPC Variables

CV1	Steam Drum Pressure
CV2	Cond. Drum Pressure
CV3	Steam Export Pressure
CV4	350-150 PRV Position
MV1	Steam Export Valve
MV2	Steam Valves to Cooler
MV3	Total Fan Speed



Heat Recovery

- Plant personnel learned about MPC application selection, MPC design and commissioning
- Identified a steam valve that had excessive leakage at shutoff
- Increase average steam export ~3000 lb/hr = \$240K/year, repair of leaking steam valve \$200K/yr benefit
- Benefit
 - Implementation time – 2 weeks
 - Benefit – \$440K/yr
 - **Payback period – 3 weeks**



Summary

- Traditional MPC is well developed, full function technology but requires a high minimum investment requiring larger projects to provide ROI
- Embedded MPC has less features but is easy to implement, low implementation cost and executes fast resulting in smaller projects to provide ROI
- Each technology has a “best fit”, so utilize each technology where they provide the best ROI



Questions